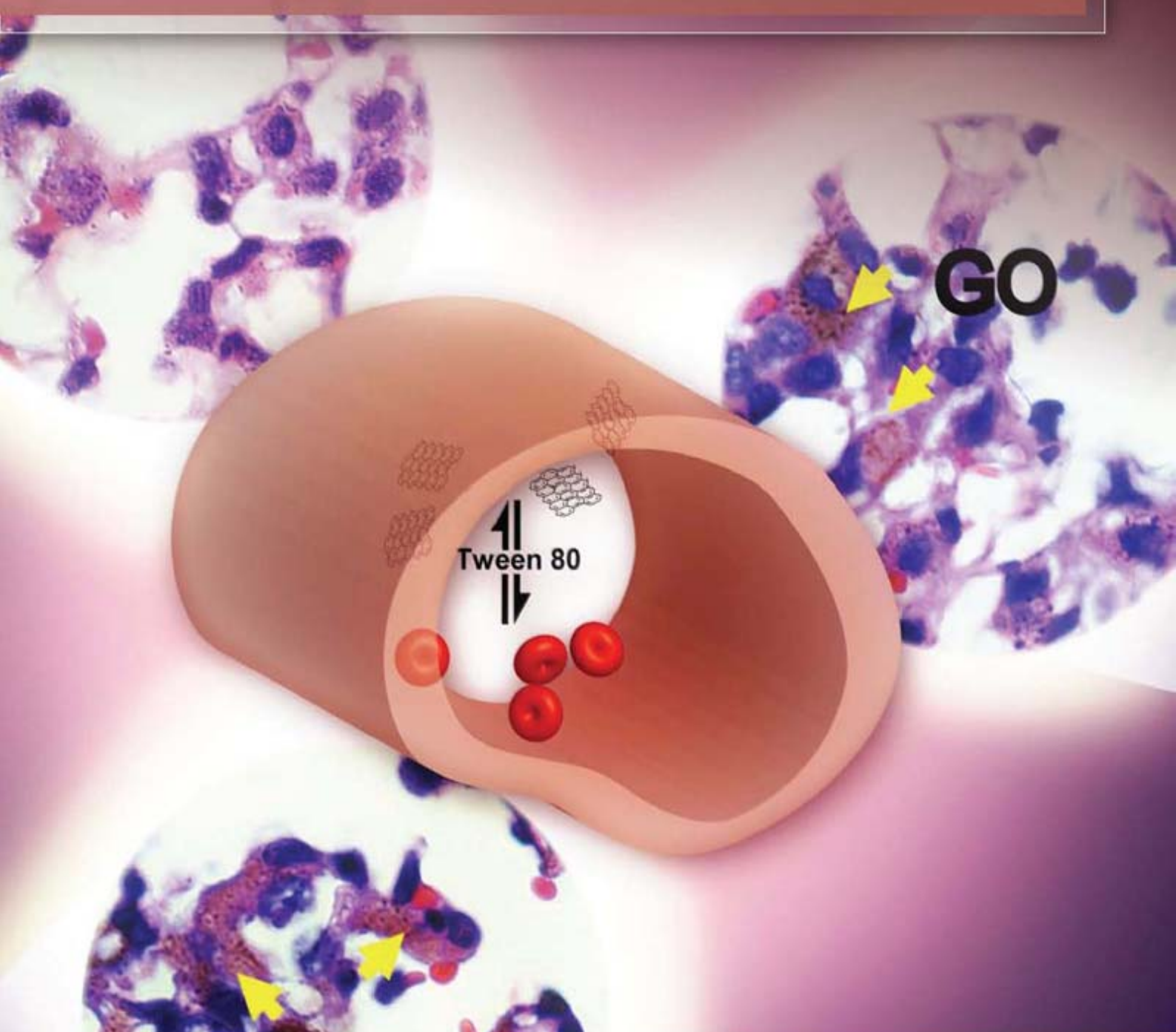


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Photo-catalytic decolourisation of toxic dye with N-doped titania: A case study with Acid Blue 25

Dhruba Chakraborty*, Susmita Sen Gupta

Department of Chemistry, B N College, Dhubri, Assam, India

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Abstract

Dyes are one of the hazardous water pollutants. Toxic Acid Blue 25, an anthraquinonic dye, has been decolourised by photo-catalysing it with nitrogen doped titania in aqueous medium. The photo catalyst was prepared from 15% TiCl_3 and 25% aqueous NH_3 solution as precursor. XRD and TEM revealed the formation of well crystalline anatase phase having particle size in the nano-range. BET surface area of the sample was higher than that of pure anatase TiO_2 . DRS showed higher absorption of radiation in visible range compared to pure anatase TiO_2 . XPS revealed the presence of nitrogen in N-Ti-O environment. The experimental parameters, namely, photocatalyst dose, initial dye concentration as well as solution pH influence the decolourisation process. At pH 3.0, the N- TiO_2 could decolourise almost 100% Acid Blue 25 within one hour. The influence of N- TiO_2 dose, initial concentration of Acid Blue 25 and solution pH on adsorption-desorption equilibrium is also studied. The adsorption process follows Lagergren first order kinetics while the modified Langmuir-Hinselwood model is suitably fitted for photocatalytic decolourisation of Acid Blue 25.

Key words: Acid Blue 25; decolourisation; nitrogen-doped titania; photocatalysis

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Introduction

Dyes are widely used in textile, leather, paper, plastic, and other industries. These are synthetic aromatic compounds containing various functional groups. The wastewater that spiked with dyes are aesthetically displeasing and also hinders the light penetration into the stream and thus results in the destruction of the aquatic ecosystem (Fu et al., 2011). Some dyes can cause allergy, dermatitis, skin irritation, mutations, and cancer in humans (Bhatnagar et al., 2009). Anthraquinonic dyes represent the second most important class of commercial dyes after azo-compounds and are mainly used for dyeing wool, polyamide and leather (Ghodbane and Hamdaoui, 2009). One of the noticeable anthraquinonic dye is Acid Blue 25, that causes skin, eye irritation and may also create respiratory problem. Thus the decontamination of this dye is major concern to the environmentalists.

Among different physical and chemical methods, heterogeneous photocatalysis assisted by various semiconductors has been considered as a cost-effective and alternative treatment process for the purification of dye-containing wastewater.

TiO_2 is considered to be the most promising photocatalyst because of its high efficiency, low cost, chemical inertness and photo-stability (Burda et al., 2003). But, due to wide band gap (3.2 eV), ultraviolet irradiation is required for photocatalytic activation of TiO_2 . It is not possible to use solar radiation efficiently using TiO_2 as photocatalyst because ultra violet radiation accounts for only about 5% of the solar radiation. In addition the high rate of electron-hole recombination on the surface and in the bulk phase of the catalyst as well as low photo-electric conversion efficiency are the hindrances for the practical applicability of TiO_2 as photocatalyst. So to make TiO_2 an effective catalyst for visible light photocatalysis some modifications are to be carried out.

One of the widely used modification methods is doping with noble and transition metals (Kemp and McIntyre, 2006; Du et al., 2008; Li et al., 2008; Sobana et al., 2008; He et al., 2010; Liu et al., 2011). However metal doping can result in thermal instability and increase in carrier trapping, which may decrease the photo catalytic efficiency (Zhu et al., 2006; Cong et al., 2007). Non-metal doping has been found to be effective to extend the photo response of TiO_2 into visible region (Sato et al., 2005; Yu et al., 2005; Cong et al., 2007). Various non metals such as B, C, N, S, F, I etc. are used for the purpose (Tachikawa et

* Corresponding author. E-mail: chakrabortydhruba@gmail.com

al., 2004; Xu et al., 2008; Ao et al., 2009; Bidaye et al., 2009; Wang and Lim, 2010; Ma et al., 2011; Wu et al., 2011). Besides, particle size also plays important role in determining the efficiency of the photocatalyst (Narayan et al., 2009). In order to maximise the photocatalytic activity, the catalyst particles should be small enough to offer higher number of active sites per unit mass. Thus the synthesis of photocatalyst in nano range has been tried as a method of modification (Zhang et al., 1998).

Asahi et al. (2001) first reported that N-doping could reduce the band gap of TiO₂ and improve its photocatalytic activity in the visible region. N-doping is widely used for developing visible light responsive TiO₂ photocatalyst for its effectiveness in narrowing the band gap (Liu et al., 2009). There are several methods for N-doping, some of which are physical methods like ion implantation (Ghicov et al., 2006; Livraghi et al., 2006), magnetron sputtering (Mwabora et al., 2004), chemical vapour deposition (Chen and Burda, 2004; Valentin et al., 2005), while the others are chemical methods, like, solvothermal process (Gandhe and Fernandes, 2005), sol-gel synthesis (Sakthivel et al., 2004; Sathish et al., 2005), chemical treatment of TiO₂ (Irie et al., 2003; Diwald et al., 2004), oxidation of titanium nitride (Livraghi et al., 2006), etc. Various titanium compounds like Ti(OCH(CH₃)₂)₄ (Wang et al., 2007), Ti(OBu)₄ (Wang et al., 2009), TiCl₄ (Li et al., 2009), TiCl₃ (Yin et al., 2005). TiO₂ (Irie et al., 2003; Silveyra et al., 2005) etc. have been used as the source of titanium. Many kinds of nitrogen sources are used as doping agent, which include urea, triethyl amine, ammonia, ammonium chloride, ammonium nitrates, hydrazine and so on (Livraghi et al., 2006; Chi et al., 2007; Cong et al., 2007; Xing et al., 2009).

In this work, nano sized (≤ 10 nm) TiO₂ has been synthesized using TiCl₃ and aqueous NH₃. The material has been found to be quite active for photochemical decolourisation of Acid Blue 25 under visible light irradiation.

1 Experimental

1.1 Materials

TiCl₃ (15%, LobaChemie) and 25% NH₃ solution (E Merck) are used as source of titanium and nitrogen respectively. The TiO₂ (anatase) was procured from Alfa Aesar. Acid Blue 25 [1-amino-9,10-dihydro-9,10-dioxo-4-(phenylamino)-2-anthracenesulfonic acid, monosodium salt] (C.I. number: 62055, molecular formula: C₂₀H₁₃N₂NaO₅S) was procured from Sigma-Aldrich and is used without further purification.

1.2 Preparation of the catalyst

A 150-mL of TiCl₃ was taken in a Teflon beaker and 100 mL aqueous NH₃ solution was added drop wise with constant stirring at 353 K. The process took about 2 hr,

after which the mixture was stirred for an additional period of 1 hr. The colour of the mixture first changed to blue and then became brownish yellow. The pH of the resulting mixture was 6.5. The solid precipitate was separated and washed with distilled water for several times and finally dried in air oven at 343 K. The sample was then calcined at 623 K for 4 hr in a muffle furnace to get a yellowish brown powder.

1.3 Characterization methods

The X-ray powder diffraction patterns of the samples are recorded on a Rigaku Miniflex diffractometer using nickle-filtered Cu K α radiation. The BET surface area of the catalysts has been measured by nitrogen adsorption method at 77 K with the help of Quantachrome Autosorb-1C surface area analyzer, using BET equation. The TEM investigation of the samples are carried out with JEOL JEM 2100 instrument operating at an accelerating voltage of 200 kV. The XPS investigation was done on ThermoScientific ESCALAB 250 instrument with monochromatized Al X-ray source. Diffuse reflectance UV-Visible spectra of the samples were obtained using a HITACHI-400 spectrophotometer.

1.4 Determination of adsorption efficiency

The adsorption experiments has been carried out in 100 mL Erlenmeyer flasks by mixing together a constant amount of catalyst dose with a constant volume of the aqueous dye solution. The contents in the flasks were agitated by placing them in a constant temperature water bath thermostat shaker for a known time interval under dark. The mixture was then centrifuged (Remi R 24) and concentration of dye solution remaining unadsorbed in the supernatant liquid has been determined with spectrometer (Elico SL 177, India) at λ_{\max} 600 nm. The adsorption parameters, namely, the influence of catalyst load (0.25 to 1.50 g/L), initial dye concentration (18.0 to 36.0 μ mol/L) and pH (3.0 to 11.0) were studied.

1.5 Determination of photocatalytic activity

The catalytic reaction was carried out in a glass reactor having water circulation facility. A 250-W halogen bulb is used as the source of visible light fitted with a glass filter to cut-off short wavelengths ($\lambda < 420$ nm). In a typical reaction 200 mL (18 μ mol/L) of the dye solution is taken with requisite amount of the catalyst and kept in dark for 60 min under stirring to attain the adsorption-desorption equilibrium. The mixture is then exposed to visible light under constant string with the help of a magnetic stirrer. The concentration of dye after adsorption (60 min) is considered as the initial concentration for photocatalytic study. Eloquent is collected at a regular interval and the concentration of the dye is measured with the help of spectrometer as before.

2 Result and discussion

2.1 Photocatalyst characterization

Figure 1 shows X-ray powder diffraction pattern of the N-TiO₂ sample which reveals formation of highly crystalline anatase titania. From the diffraction pattern, the presence of any other phase is ruled out. The particle size of N-TiO₂ has been calculated from the (101) peak with the help of Scherrer equation (Lin et al., 2002; Cong et al., 2007):

$$D = k\lambda/\beta\cos\theta \quad (1)$$

where, $k = 0.9$, $\lambda = 0.154$ nm, β = full width half maxima and θ = diffraction angle. The calculated value of the particle size of N-TiO₂ and TiO₂ was approximately 6.2 and 12 nm, respectively.

The diffused reflectance spectra of N-TiO₂ and TiO₂ are shown in **Fig. 2**. It can be seen that the visible light absorption is higher in the case of N-TiO₂ and it extends to about 600 nm. The band gap energy (E_g) was calculated on

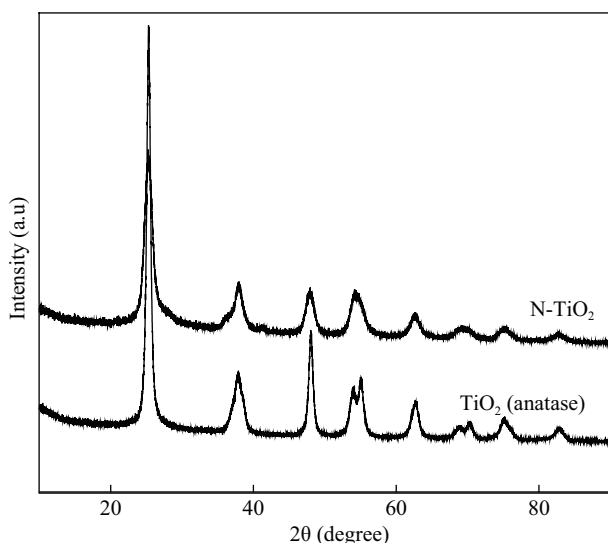


Fig. 1 XRD patterns of N-TiO₂.

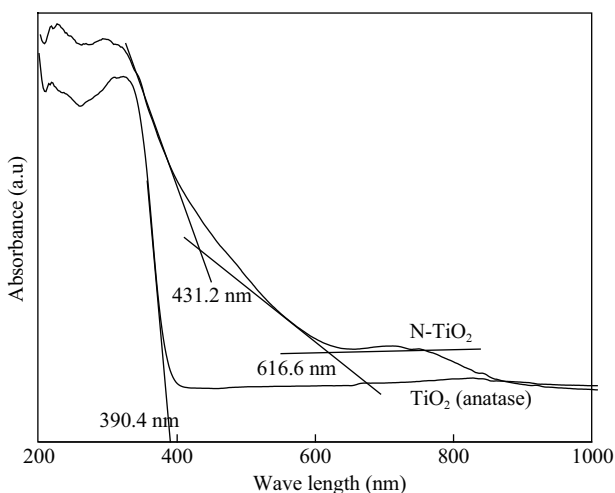


Fig. 2 UV-Vis diffuse reflectance spectra of N-TiO₂.

the basis of the equation $E_g = 1240/\lambda$ (Shao et al., 2008), λ (nm) is the wavelength value corresponding to the point of intersection between the vertical and the horizontal line in the spectra. The band gap energy for TiO₂ was found to be 3.17 eV. On the other hand in N-TiO₂, there are two band gap at 2.87 and 2.01 eV. The former band gap should be due to TiO₂ environment while the later one must have resulted from N-doping. There is red shift of minimum 0.3 eV in the N-TiO₂ sample compared to the TiO₂ sample. The narrower band gap is responsible for excitation of an electron from the valence band to the conduction band in N-TiO₂ and thus increases the photocatalytic activity of the material.

The TEM image of the N-TiO₂ is shown in **Fig. 3**. It can be seen that the crystallites agglomerated to larger particles. The images reveal that the sample consists of agglomerates of primary particles with the crystallite size ranging from about 6 to 10 nm which is in good agreement with the crystallite size calculated from XRD pattern. The diffraction patterns show the characteristics lines of anatase phase of TiO₂, which is in agreement with the XRD analysis.

The BET surface area of the sample was measured to be 176 m²/g, the BET surface area of the TiO₂ (anatase) is 150 m²/g.

Figure 4 shows XPS spectra of N1s electron with binding peak at the binding energy of 400 eV. The N concentration in the sample is about 0.20%. From the XPS results of different groups it has been observed that there is no consensus on the assignment of the N1s binding energy for nitrogen doped TiO₂. Generally there are two kinds of XPS peak observed in N-doped TiO₂. One with its binding energy around 397 eV is considered to be originating from nitrogen in Ti–N bond due to its proximity to the typical binding energy of Ti–N at 397.2 eV (Saha and Tomkins, 1992). The other with higher binding energy near 400 eV has been assigned by different groups to N1s in O–Ti–N environment. Satish et al. (2005) attributed a peak at 398.2 eV to N⁻ anion incorporated in the TiO₂ as N–Ti–O structural feature. Li et al. (2009) also attributed the peak at binding energy 398.6 eV to the N1s electron in N–Ti–O structure. Cong et al. (2007) observed two kinds of N-species with their binding energies 399.2 and 401.2 eV which were assigned to N–Ti–O and Ti–O–N linkages respectively. In their N-doped TiO₂ samples, Liu et al. (2009) observed peaks in the range 399.6 to 399.9 eV and attributed them to N–Ti–O form of nitrogen. Chen and Burda (2004), on the other hand, attributed the peak at 401.3 eV to nitrogen in the N–Ti–O environment. Thus different groups attributed different binding energies to N1s in N–Ti–O environment. The variation may be due to different preparation procedures adopted by the different groups. The N1s binding energy is higher when formal charge of N is more positive (Chen and Burda, 2004). When nitrogen forms N–Ti–O linkage, the electron density

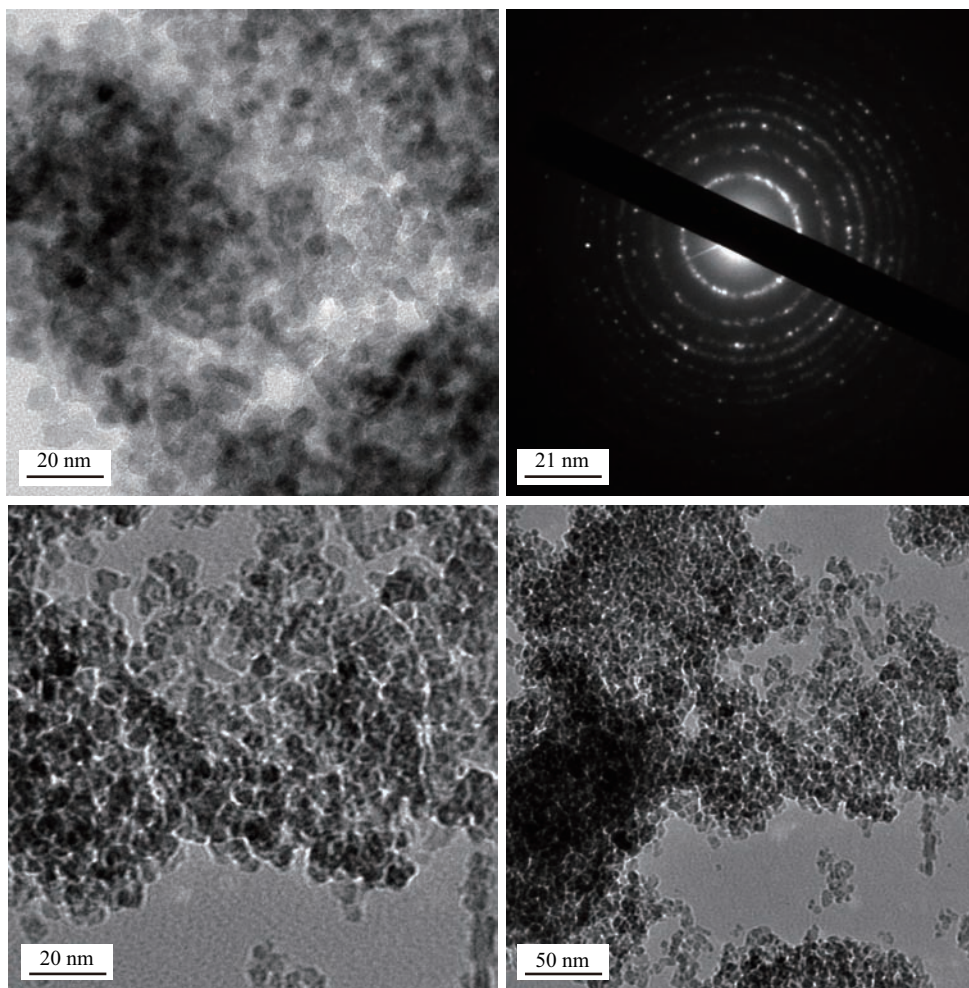


Fig. 3 TEM image of N-TiO₂ at different magnification.

around the nitrogen atom decreases compared to that in N-Ti-N of TiN because of the O atom. Thus, the N1s binding energy in N-Ti-O is higher than that in N-Ti-N. On the basis of above discussion we think the N1s binding energy peak at 400 eV in our sample is most probably due to O-Ti-N environment.

2.2 Adsorption capacity of Acid Blue 25 on N-TiO₂

2.2.1 Influence factors

The influence of amount of N-TiO₂ on the adsorption of Acid Blue 25 has been studied. For any fixed dose of N-TiO₂, the uptake increases and attains equilibrium within 60 min. At equilibrium (initial dye concentration 18 μmol/L), the adsorption increases from 7.1% to 34.4% for N-TiO₂ dose of 0.25 g/L to 1.0 g/L. The higher amounts of titania provide more surface for the dye to get adsorbed on it. However, further increase of adsorbent dose (1.5 g/L) decreases the extent of adsorption which may be due to particle agglomeration. **Figure 5a** represents the C_t/C_0 vs. t plots for different doses of N-TiO₂.

The initial dye concentration was studied by increasing the initial concentration of dye from 18.0 to 36.0 μmol/L,

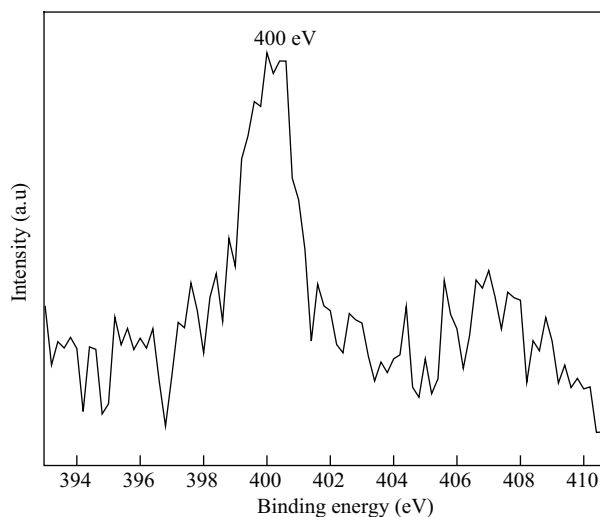


Fig. 4 XPS spectra of N-TiO₂.

the extent of adsorption varies from 10.5% to 13.2%. The initial higher uptake has been observed for first 10 min and equilibrium is attained within 60 min for all the cases (**Fig. 5b**).

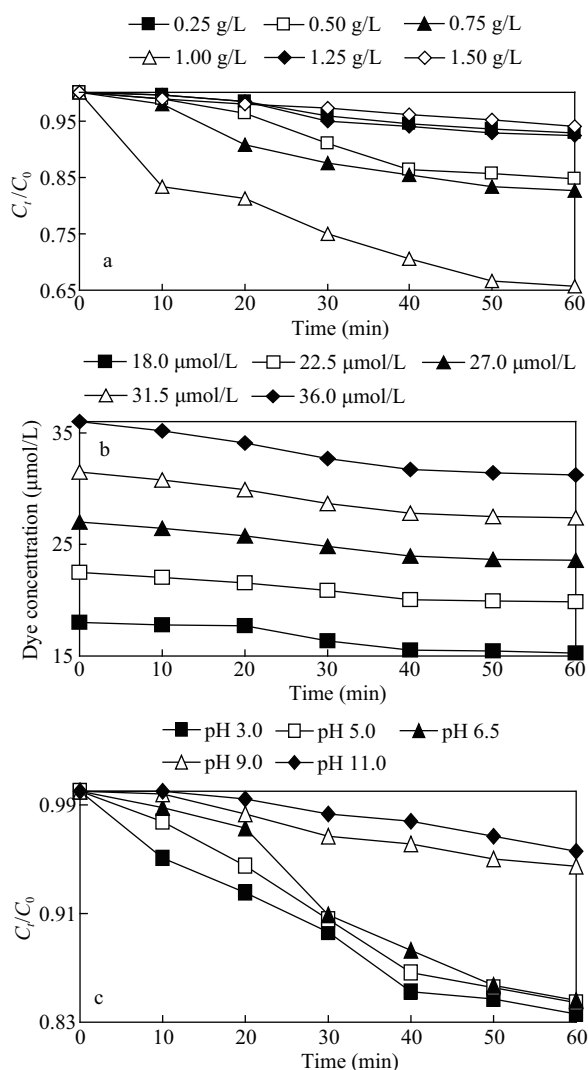


Fig. 5 Influence of N-TiO₂ dose (a), initial Acid Blue 25 concentration (b) and solution pH (c) on the adsorption of dye on N-TiO₂ at 303 K.

The pH of the aqueous solution is a significant controlling factor in adsorption mechanism. For 1.0 g/L of N-TiO₂ and initial dye concentration of 18 μmol/L, the extent of adsorption is maximum (16.3%) at pH 3.0 and showed a steady decrease upto pH 9.0 (4.0%) (**Fig. 5c**). At acidic pH, a significantly high electrostatic attraction exists between the positively charged surface of the N-TiO₂ and the anionic dye. As the pH of the system increases, the surface charge turns towards negative and adsorption of dye anions comes down (Bulut et al., 2008). Moreover, at high pH, there may be competition between OH⁻ and coloured ions of Acid Blue 25 for negatively charged adsorption sites on the surface of the adsorbent and the highly mobile OH⁻ ions are likely to be preferentially adsorbed in comparison to the bulky dye anions.

2.2.2 Adsorption isotherms

The adsorption of the dye on the pure and N doped TiO₂ has been studied by the well known Langmuir isotherm given by (Langmuir, 1918):

$$C_e/q_e = (1/bq_m) + (1/q_m)C_e \quad (2)$$

where, C_e and q_e are the concentration of dye and amount of dye adsorbed per unit mass of adsorbent at equilibrium respectively, q_m is the Langmuir monolayer adsorption capacity. The linear Langmuir plots are obtained by plotting C_e/q_e vs. C_e . The q_m values are calculated as 2.55×10^{-4} and 1.30×10^{-3} mg/g for pure and modified TiO₂, respectively.

2.2.3 Adsorption kinetics

The adsorption of Acid Blue 25 is studied by using Lagergren pseudo first-order model (Lagergren, 1898; Ho, 2004):

$$\log(q_e - q_t) = \log q_e - k_1 t \quad (3)$$

where, q_e and q_t are the amounts adsorbed per unit mass at equilibrium and at any time t , k_1 is the first order adsorption rate constant. For different doses of N-TiO₂, the $\log(q_e - q_t)$ vs. t plots (**Fig. 6a**) are linear (r : 0.885–0.991) and the first order rate constants (obtained from the slopes) varies from 6.12×10^{-2} to 7.48×10^{-2} min⁻¹ for N-TiO₂ dose. Similarly, the k_1 values are in the range of 6.31×10^{-2} to 10.36×10^{-2} min⁻¹ (r : 0.926~–0.969) for the variation of initial dye concentration from 18 to 36.0 μmol/L (**Fig. 6b**) and 6.60×10^{-2} to 3.33×10^{-2} min⁻¹ as the solution pH changed from 3.0 to 11.0 (r : –0.957~–0.976) (**Fig. 6c**). All the k_1 values are listed in **Table 1**.

Table 1 Lagergren first order rate constants for adsorption of Acid Blue 25 on N-TiO₂

N-TiO ₂ dose (g/L)	$k_1 \times 10^2$ (min ⁻¹)	Initial Acid Blue 25 conc. (μmol/L)	$k_1 \times 10^2$ (min ⁻¹)	pH	$k_1 \times 10^2$ (min ⁻¹)
0.25	6.12	18.0	6.31	3.0	6.60
0.50	6.31	22.5	8.47	5.0	6.58
0.75	7.16	27.0	8.54	6.5	6.31
1.00	7.48	31.5	8.72	9.0	5.46
1.25	5.91	36.0	10.36	11.0	3.33
1.50	3.73				

2.3 Photocatalytic decolourisation of Acid Blue 25 on N-TiO₂

2.3.1 Influence factors

Figure 7a shows the degradation profile of Acid Blue 25 with an initial concentration of 18 μmol/L under various catalyst loadings. The results reveal that the decolorizing efficiency shows increasing trend with the increase in N-TiO₂ loading from 0.25 to 1.25 g/L. The change in percentage decolourisation is maximum when catalyst amount is changed from 0.25 g/L (77.1% at 180 min)

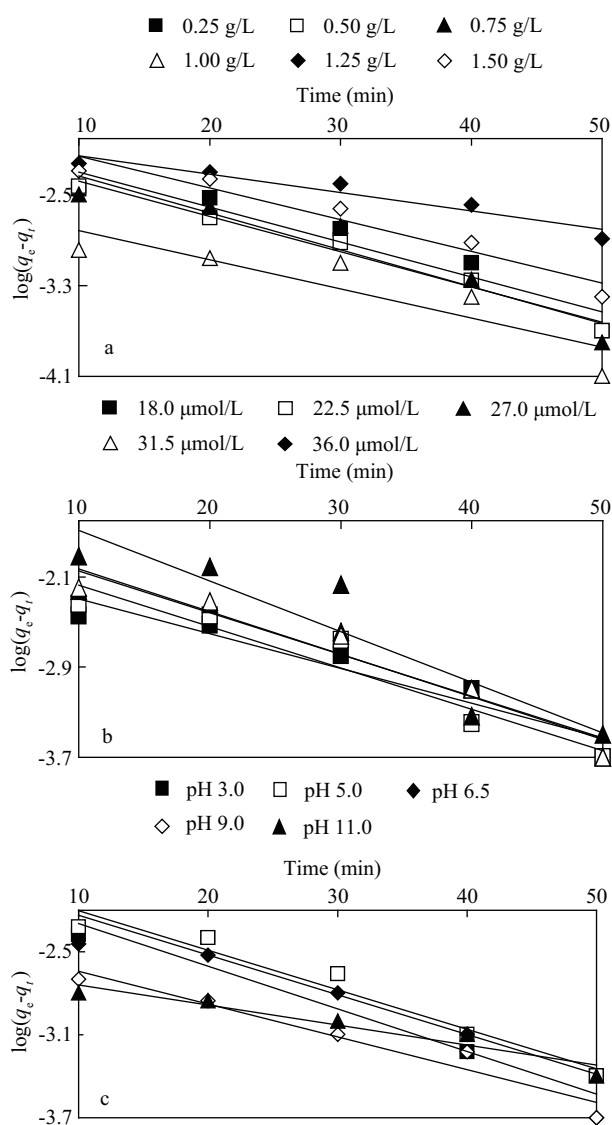


Fig. 6 Lagergren plots for adsorption of Acid Blue 25 on N-TiO₂ for the variation of N-TiO₂ dose (a), initial Acid Blue 25 concentration (b) and solution pH (c).

to 0.5 g/L (88.8% at 180 min) compared to rest of the N-TiO₂ load (for 0.75 g/L: 89.9%, 1.0 g/L: 95.3%, 1.25 g/L: 95.8% (at 180 min)). However, the increase in N-TiO₂ loading above 1.25 g/L shows a decreasing trend in percentage decolourisation of Acid Blue 25 (for 1.5 g/L: 89.3% at 180 min). The increase of catalyst load beyond the optimum amount may result in the agglomeration of catalyst particles, and thus make a part of the catalyst surface become unavailable for light absorption, which lowers the efficiency of decolourisation (Huang et al., 2008). It has also been reported that as the excess catalyst prevent the illumination, concentration of OH radical, a primary oxidant in the photocatalytic system decreases which in turn decreases the efficiency of the dye decolourisation (Sun et al., 2008). Similar results were reported earlier (Nagaveni et al., 2004; Liu et al., 2006; Saquiba et al., 2008).

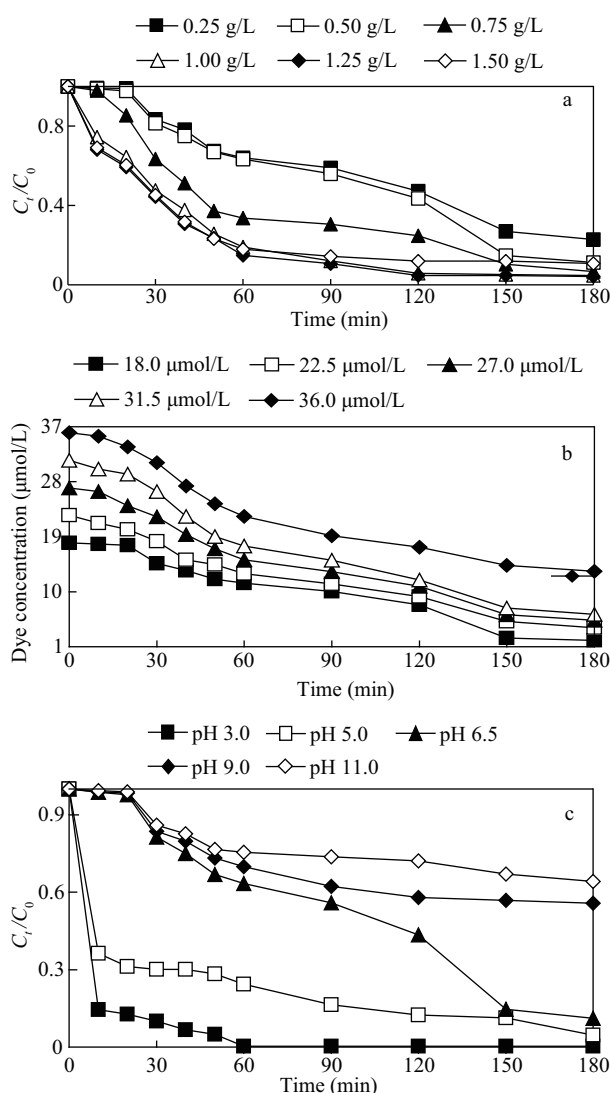


Fig. 7 Influence of N-TiO₂ dose (a), initial Acid Blue 25 concentration (b) and solution pH (c) on the decolourisation of dye on N-TiO₂ at 303 K.

Figure 7b represents the effect of initial concentration of Acid Blue 25 on the decolourisation efficiency of N-TiO₂. For any concentration of the dye, rapid uptake takes place in the first 60 min and equilibrium was attained within 180 min. It can be seen from the **Fig. 7b** that the concentration has a significant effect on the degradation of dye.

The effect of solution pH on the efficiency of N-TiO₂ for decolourisation of Acid Blue 25 has been studied in the pH range of 3.0 to 11.0 (**Fig. 7c**). The study reveals that the extent of decolourisation increases with decrease in pH. At pH 3.0, 0.5 g/L N-TiO₂ can decolourise almost 100% Acid Blue 25 (initial concentration 18 μmol/L) within 60 min. It has been reported that acid-base properties of the metal oxide surfaces can have considerable implications upon their photocatalytic activity (Bahnemann et al., 1994). The formation of the electrical double layer at the solid-electrolyte interface affects the sorption-desorption processes and thus separate the photogenerated electron-

hole pairs at the surface of the semiconductor particles. Acid Blue 25 is an anionic dye having a sulphonate group and its adsorption is favoured at low pH (Sleiman et al., 2007) which may help the decolourisation reaction. Similar results were reported by other authors as well (Sleiman et al., 2007; Zhiyon et al., 2007).

2.3.2 Kinetics of photocatalytic degradation

The kinetics of the Acid Blue 25 decolourisation has been studied by modified Langmuir-Hinselwood (L-H) mechanism, given by Eq. (4):

$$-dc/dt = (kK_e C)/(1 + K_e C) \quad (4)$$

where, C is the concentration of dye, k (min^{-1}) is the apparent reaction rate constant, K_e is the apparent equilibrium constant for the adsorption of the dye on the catalyst surface.

Eq. (4) can be written as:

$$t = 1/(K_e k) \ln(C_0/C) + (1/k)(C_0 - C) \quad (5)$$

For the sufficient low concentration of dye, Eq. (5) can be expressed as:

$$\ln(C_0/C) = kK_e t = k' t \quad (6)$$

where, k' (min^{-1}) is the overall rate constant. By plotting $\ln(C_0/C)$ as a function of irradiation time through regression, we obtained for each catalyst sample the k' (min^{-1}) constant from the slopes.

The overall rate constant for Acid Blue 25 decolourisation on N-TiO₂ has been studied for the variation of catalyst load, initial dye concentration and solution pH. All the plots can be roughly considered as straight line (Fig. 8). The rate constants increase from $8.6 \times 10^{-3} \text{ min}^{-1}$ (catalyst load 0.25 g/L) to $17.8 \times 10^{-3} \text{ min}^{-1}$ (catalyst load 1.25 g/L) and then decrease to $10.9 \times 10^{-3} \text{ min}^{-1}$ for N-TiO₂ of 1.50 g/L, which indicates that the decolourisation rates depend on the catalyst amount. For different dye concentrations, the rate constant varies from 12.6×10^{-3} to $6.2 \times 10^{-3} \text{ min}^{-1}$ as the concentration of Acid Blue 25 changes from 18.0 to 36.0 $\mu\text{mol/L}$, which is consistent with the influence of variation of dye concentration on photocatalytic decolourisation. Similarly, the overall rate constant calculated at different pH are: $k'_{\text{pH } 3.0}$ (64.5×10^{-3}) > $k'_{\text{pH } 5.0}$ (13.1×10^{-3}) > $k'_{\text{pH } 6.5}$ (12.6×10^{-3}) > $k'_{\text{pH } 9.0}$ (3.5×10^{-3}) > $k'_{\text{pH } 11.0}$ (2.3×10^{-3}), which indicates that the decolourisation rate are pH dependent and lower pH favours the process more efficiently. All the values of degradation rate are given in the Table 2.

2.4 Comparison of decolourisation of Acid Blue 25 on N-TiO₂ with that of pure TiO₂ (anatase)

The decolourisation of Acid Blue 25 by N-TiO₂ has been compared with pure TiO₂ (anatase) (Fig. 9). It is found

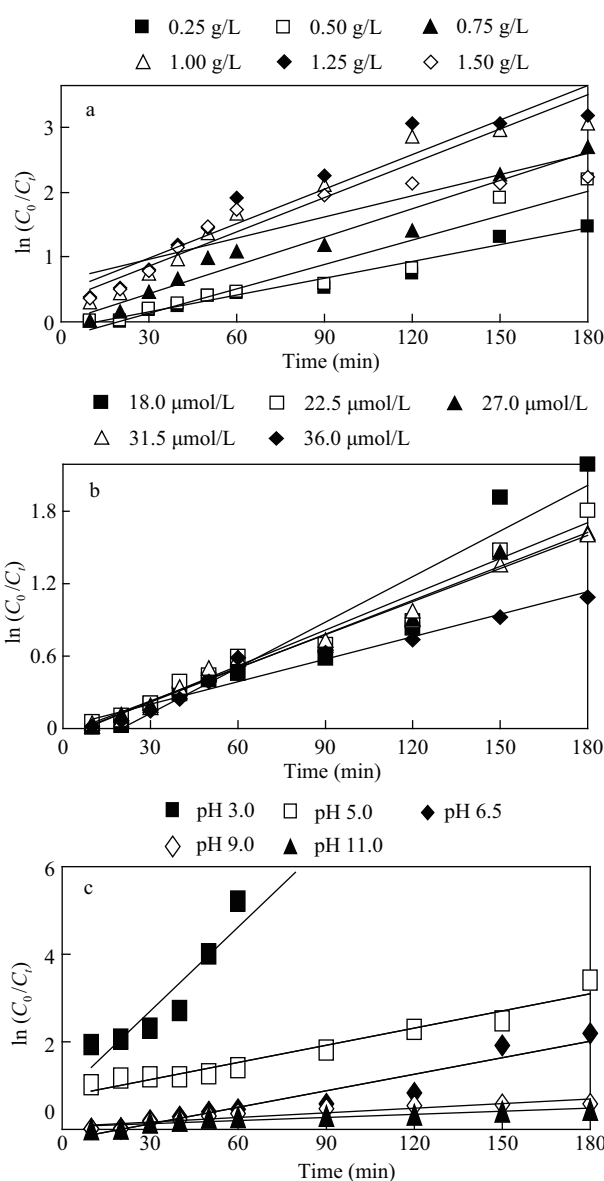


Fig. 8 Langmuir-Hinselwood plots for Acid Blue 25 degradation on N-TiO₂ for the variation of N-TiO₂ dose (a), initial acid blue concentration (b) and solution pH (c).

Table 2 Langmuir-Hinselwood first order rate constants for adsorption of Acid Blue 25 on N-TiO₂

N-TiO ₂ dose (g/L)	$k' (\times 10^3 \text{ min}^{-1})$	Initial Acid Blue 25 conc. ($\mu\text{mol/L}$)	$k' \times 10^3 (\text{min}^{-1})$	pH	$k' \times 10^{-3} (\text{min}^{-1})$
0.25	8.6	18.0	12.6	3.0	64.5
0.50	12.6	22.5	9.9	5.0	13.1
0.75	14.5	27.0	9.4	6.5	12.6
1.00	17.6	31.5	9.1	9.0	3.5
1.25	17.8	36.0	6.2	11.0	2.3
1.50	10.9				

that, at 180 min (initial dye concentration: 18 $\mu\text{mol/L}$), 0.5 g/L of N-TiO₂ can decolourise 88.8% of Acid Blue 25 whereas only 12.7% dye decolourisation is done by TiO₂

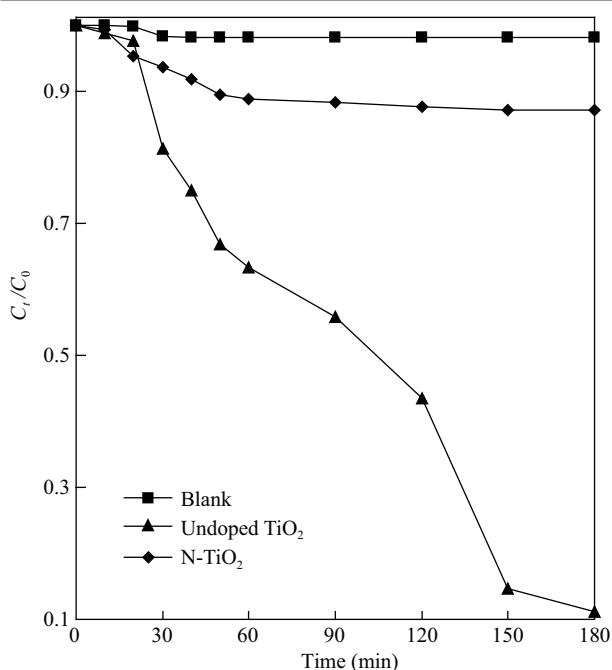


Fig. 9 Comparison of the photocatalytic degradation of Acid Blue 25 by undoped TiO₂ and N-TiO₂. Initial concentration of dye 18.0 μmol/L, catalyst load 1.0 g/L, temperature 300 K.

(under similar conditions). Thus, the modified TiO₂ can decolourise Acid Blue 25 almost 7 times more than pure TiO₂ (anatase). The blank experiment that has been carried out with the dye in absence of catalyst under visible light, reveals that a very negligible amount of decolourisation (2.2 %) has occurred (**Fig. 9**).

It is also found that the Langmuir-Hinselwood rate constant of Acid Blue 25 decolourisation by N-TiO₂ is ca. 21 times higher compared to the rate constant of the dye decolourisation by undoped TiO₂ under similar experimental conditions (k' for N-TiO₂: $12.6 \times 10^{-3} \text{ min}^{-1}$; TiO₂: $6.0 \times 10^{-4} \text{ min}^{-1}$).

3 Conclusions

Acid Blue 25 can be efficiently decolourised by visible light photocatalysis with nitrogen doped titania. The nitrogen doped nanocrystalline titania synthesized by a very simple method using TiCl₃ and aqueous NH₃ shows greater absorption of visible radiation and a red shift in the band gap energy compared to pure anatase TiO₂. The doped TiO₂ contains nitrogen in N-Ti-O environment. Both adsorption as well as photocatalytic decolourisation of Acid Blue 25 has been influenced by experimental variables, namely, N-TiO₂ dose, initial dye concentration and solution pH. The decolorization efficiency increases with the increase in N-TiO₂ load from 0.25 to 1.25 g/L and then again decreases when the load is 1.5 g/L. The decrease of solution pH increases the decolourisation of dye and at pH 3.0, almost 100% Acid Blue 25 is decolourised (0.5 g/L N-TiO₂, initial concentration 18 μmol/L) within 60 min.

The modification of TiO₂ improved the decolourisation compared to pure TiO₂ (anatase) as the N-TiO₂ decolourised the dye almost 7 times more compared to undoped TiO₂. The higher visible light photo-catalytic activity of N-TiO₂ is possibly due to the fact that nitrogen doping effectively inhibits the recombination of the electron and the holes. Besides the higher absorption in the visible-light range and a red shift in the band gap indicates that more photoinduced electrons and holes could participate in the photocatalytic reactions in N-TiO₂ compared to TiO₂. The kinetics of dye decolourisation closely follows modified Langmuir-Hinshelwood (L-H) mechanism.

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