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# Through converting the surface complex on TiO<sub>2</sub> nanorods to generate superoxide and singlet oxygen to remove CN<sup>-</sup>

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## ABSTRACT

Cyanide (CN<sup>-</sup>) is extensively used in the process of plating devices and for surface treatment in the electroplating industry and is extremely hazardous to humans and the environment. Peroxymonosulfate (PMS)-based advanced oxidation processes (AOPs) hold considerable promise for CN<sup>-</sup> removal. However, the activity of sulfate radical and hydroxyl radical generated in the PMS activation process is low in the base condition, leading to a drop in its efficiency in CN<sup>-</sup> removal. Thus, a photo-electrocatalytic system (PEC), developed using a TiO<sub>2</sub> photoanode and a carbon aerogel cathode, was used to activate PMS for the removal of CN<sup>-</sup> from wastewater through the generation of radicals and non-radicals. The PEC/PMS system could effectively remove CN<sup>-</sup>, with the removal efficiency reaching 98.5% within 2 min, when PMS concentration was at the 0.25 mmol/L level, and the applied bias voltage was -0.5 V. The main active species in the PEC/PMS system were superoxide radicals and singlet oxygen, which was proved through electron paramagnetic resonance detection and quenching experiments. Results obtained through *in-situ* Raman measurements, photocurrent tests, and electrochemical impedance spectroscopy measurements indicated that the TiO<sub>2</sub> could activate PMS to generate active species. Following many cycles of experimentation, it was discovered that the system displayed high catalytic performance and possessed satisfactory stability to remove CN<sup>-</sup> economically and efficiently.

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## Introduction

Cyanide (CN<sup>-</sup>) is extensively used in the process of plating devices and for surface treatment in the electroplating industry due to its robust complexing ability with metal ions (Adams et al., 2020; Monser and Adhoum, 2002), leading to a

large concentration of residual CN<sup>-</sup> being found in wastewater generated from the electroplating process. The presence of CN<sup>-</sup> in waters even at low concentration of 0.04–0.1 mg/L damages significantly fish and other aquatic organisms. Untreated electroplating wastewaters contain usually high amounts of CN<sup>-</sup>, even much higher than the recommended concentration, which poses a serious threat to the environment and human health. Therefore, the intensification of technologies towards CN<sup>-</sup> removal from wastewater is

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very recommended to maintaining water security and human health.

A variety of methods have been developed to eliminate  $\text{CN}^-$  from wastewater including alkaline chlorination (Lv et al., 2015), electro dialysis (Zheng et al., 2015), electrocatalysis (Wang et al., 2017), and photo-electrocatalysis (Mao et al., 2019; Dong et al., 2021; Tian et al., 2018). Additionally, the persulfate-based advanced oxidation processes (AOPs) enable the efficient degradation of  $\text{CN}^-$  due to the strong oxidation ability of sulfate radicals ( $\text{SO}_4^{\cdot-}$ ) produced in the process (Zhu et al., 2019; Deng et al., 2018). Peroxydisulfate (PDS) and peroxy-monosulfate (PMS) are two typical persulfates, with PMS possessing the potential to be readily activated to yield  $\text{SO}_4^{\cdot-}$  due to its asymmetric structure (Duan et al., 2016; Song and Liu, 2018), thus garnering more attention than PDS.  $\text{SO}_4^{\cdot-}$  possesses high oxidation potential (2.8–3.0 eV) and a long half-life (30–40  $\mu\text{sec}$ ) (Wang et al., 2018), resulting in its high efficacy in the degradation of pollutants. Apart from  $\text{SO}_4^{\cdot-}$ , PMS can be converted and used to produce other strong oxidizing active species such as hydroxyl radicals ( $\cdot\text{OH}$ ) (Duan et al., 2018; Gao et al., 2018), superoxide radicals ( $\text{O}_2^{\cdot-}$ ) (Han et al., 2020; Li et al., 2020), and singlet oxygen ( $^1\text{O}_2$ ) (Duan et al., 2020; Fan et al., 2019), all of which could be effectively used for the degradation of pollutants in wastewater.

The activation of PMS to generate active species is dependent on external factors, with the commonly used methods at present being energy transfer (including heat, UV, and ultrasound) and transition metal activation (Chen et al., 2019; Ao et al., 2018; Wang and Wang, 2018). The  $\text{SO}_4^{\cdot-}$  and  $\cdot\text{OH}$  generated through these processes could be used to remove organic pollutants. However,  $\text{SO}_4^{\cdot-}$  and  $\cdot\text{OH}$  could also be expended by other species, such as anion  $\text{Cl}^-$ ,  $\text{HCO}_3^-$ ,  $\text{CO}_3^{2-}$ , and  $\text{NO}_3^-$  (Jawad et al., 2020), forming  $\text{Cl}\cdot$ ,  $\text{HCO}_3^{\cdot-}$ ,  $\text{CO}_3^{2-\cdot}$ , and  $\text{NO}_3^{\cdot-}$ , and the oxidizing capacity of these newly formed radicals would be too low to remove pollutants. Moreover, researchers would also need to consider the drawbacks to this method such as excessive energy inputs and transition metal ions leaching out. Therefore, it was imperative that an economical and efficient method to activate PMS be developed. Recent research indicated that the use of photoelectric catalysts and carbon materials was an excellent mode of activating PMS to produce non-radicals (Chen et al., 2021; Qin et al., 2020). Among the photoelectric catalysts,  $\text{TiO}_2$  was one of the most significant semiconductor photocatalysts due to its light corrosion resistance and photochemical stability. Previous study indicated that PMS activation could be enabled through a ligand-to-metal charge transfer (LMCT) mechanism (Joa et al., 2018). Although carbonaceous materials have showed excellent catalytic PMS activation, among them carbon aerogel (CA) based materials have showed many unique properties due to the three-dimensional network structure which could intensity the catalytic efficiency (Wang et al., 2013).

Having been enlightened by previous researchers, a photoelectrocatalytic (PEC) system, constructed using  $\text{TiO}_2$  as the photoanode and CA as the cathode, was used to activate PMS and achieve  $\text{CN}^-$  removal in this study. The generation of non-radicals during the PMS activation process in the inherent strong base condition ( $\text{CN}^-$  would escape into the air when the pH value was as low as 9) via conversion of surface com-

plexes, was expected. The removal process was optimized by studying the influence of different PMS concentrations, photocatalysis, electrocatalysis, and the applied bias voltage on the activation of PMS, and then the reaction kinetic in the process of  $\text{CN}^-$  removal using the PEC/PMS method was explored. Furthermore, the removal mechanism and active species were studied by conducting electron paramagnetic resonance (EPR) tests and quenching experiments. Finally, the effect of  $\text{TiO}_2$  on PMS activation was analyzed using the *in-situ* Raman test, photocurrent density, and electrochemical impedance spectroscopy (ESI). Overall, this work offered an emerging and promising method to activate PMS and generate active species to treat  $\text{CN}^-$ -contaminated wastewater.

## 1. Materials and methods

### 1.1. Reagents

Tetra-*n*-butyl titanate ( $\text{C}_{16}\text{H}_{36}\text{O}_4\text{Ti}$ , analytical reagent (AR), 98.0 wt.%), hydrochloric acid (HCl, guaranteed reagent (GR), 36.0–38.0 wt.%), absolute ethanol ( $\text{C}_2\text{H}_5\text{OH}$ , GR, 99.0 wt.%), chloramine T trihydrate ( $\text{C}_7\text{H}_7\text{ClNNaO}_2\text{S}\cdot 3\text{H}_2\text{O}$ , AR, (Cl) 24.0 at.%), isonicotinic acid ( $\text{C}_6\text{H}_5\text{NO}_2$ , chemical pure (CP), 98.0 wt.%), barbituric acid ( $\text{C}_4\text{H}_4\text{N}_2\text{O}_3$ , AR, 99.0 wt.%), potassium monopersulfate triple salt (PMS,  $\text{KHSO}_5$ , 47.0 wt.%), resorcinol ( $\text{C}_6\text{H}_6\text{O}_2$ , AR, 99.0 wt.%), formaldehyde ( $\text{CH}_2\text{O}$ , 37.0 wt.%), sodium carbonate ( $\text{Na}_2\text{CO}_3$ , AR, 98 wt.%), sodium cyanide ( $\text{NaCN}$ , AR, 98.0 wt.%) and sodium hydroxide ( $\text{NaOH}$ , AR, 96.0 wt.%) were bought from Sinopharm Chemical Reagent Co., Ltd; Methanol ( $\text{CH}_3\text{OH}$ , high pressure liquid chromatography (HPLC) grade  $\geq 99.9$  wt.%) and acetone ( $\text{C}_3\text{H}_6\text{O}$ , AR, 98.0 wt.%) were purchased from Thermo Fisher scientific Co., Ltd.; Nessler reagent (AR), were obtained from Sigma Reagent Co., Ltd.; Potassium sodium tartrate tetrahydrate ( $\text{C}_4\text{H}_4\text{O}_4\text{KNa}\cdot 4\text{H}_2\text{O}$ , AR, 98.0 wt.%) was purchased from Shanghai Macklin biochemical co., Ltd. All the reagents have not been further purification.

### 1.2. Preparation

#### 1.2.1. Preparation of $\text{TiO}_2$ nanorods (NRs)

The synthesis of  $\text{TiO}_2$  NRs by hydrothermal method was carried out based on previous report (Xie et al., 2013): 45 mL of HCl and 45 mL of ultrapure water were added into a beaker and stir for 5 min. Subsequently, 1.5 mL of tetra-*n*-butyl titanate was dropwise added to the mixed solution, and the mixture was transferred to a polytetrafluoroethylene reactor after thorough stirring. Then the clean fluorine-doped tin oxide (FTO) glass was immersed in the mixture obliquely with the conductive surface facing up, the reactor was transferred to an oven, and reacted at 150°C for 5 hr. During the reaction,  $\text{TiO}_2$  will grow on the conductive surface of the FTO glass and cool to 20–25°C after the reaction. Then take out the FTO glass grown with  $\text{TiO}_2$ , rinse it with ultrapure water 3 times, and dry it naturally to obtain pure  $\text{TiO}_2$ . After drying, the FTO glass grown with  $\text{TiO}_2$  was placed in a muffle furnace at 500°C and calcined for 2 hr at a heating rate of 2.5°C/min to obtain  $\text{TiO}_2$  NRs.

### 1.2.2. Preparation of CA

CA was synthesized using the procedure reported in previous study (Wang et al., 2013). Resorcinol (55 g) was added to 98.5 mL of ultrapure water in a beaker, the mixture was stirred for 30 min. Formaldehyde (72.5 mL) and 4.24 g/L  $\text{Na}_2\text{CO}_3$  (10 mL) were sequentially added and stirred for 30 min. Afterwards, the mixture was transferred to the prepared mold, and then the mold was wrapped with plastic wrap, and placed in the oven. It was reacted at 30 and 50°C for 1 day, respectively, and at 90°C for 3 days. Then, the plastic wrap was removed and the cured material was taken out, sand the material and soaked it in acetone for 3 days (the acetone needs to be replaced every day). After that, take out the material and place it in a fume hood to dry naturally. The dried material was put into a tube furnace with the protection of  $\text{N}_2$  to carbonization at 950°C for 4 hr and the heating rate is 2.5°C/min. Then it was cooled to 20–25°C to obtain black solid CA.

### 1.3. Experimental procedure

$\text{NaCN}$  solution (44.4 mg/L, 100 mL) was placed into the reactor with magnetic stirring, then adjusted the pH using 10 g/L and 1.0 g/L  $\text{NaOH}$  and kept the pH around 12. The PEC/PMS system was constructed with  $\text{TiO}_2$  as the counter electrode, CA as the working electrode and calomel electrode as the reference electrode. The distance between the lamp and the reactor was kept 10 cm. A 300 W luminous power Xe lamp (Perfect Light technology Co., LTD, Beijing) was used as source for light. Sodium chloride ( $\text{NaCl}$ ) and PMS were added to the  $\text{NaCN}$  solution, respectively, to study the effect of different additives on the degradation of cyanide. And the effects of different concentrations of PMS, applied bias and photocatalysis were studied separately. Sample (1.0 mL) was taken at 0, 0.3, 0.6, 1, 2, 5, and 10 min to detect the  $\text{CN}^-$  concentration.

### 1.4. Analytical methods

#### 1.4.1. $\text{CN}^-$ concentration detection

The concentration of  $\text{CN}^-$  was detected by isonicotinic acid-barbituric acid UV-Vis spectrophotometry (Wang et al., 2017; Gao et al., 2013). Under weak acid conditions,  $\text{CN}^-$  can react with chloramine-T to form cyanogen chloride, which then react with isonicotinic acid to form glutaraldehyde. The glutaraldehyde can form a blue-violet complex with barbituric acid, and the chroma of the complex is proportional to the concentration of  $\text{CN}^-$  within a certain range. The concentration of  $\text{CN}^-$  can be calculated through the calibration curve.

#### 1.4.2. $\text{CNO}^-$ concentration detection

$\text{CNO}^-$  can be hydrolyzed to carbonate and ammonium under acidic conditions, so we can detect the concentration of ammonium to indirectly analyzed the concentration of  $\text{CNO}^-$  through the Nesslerization method (Guo et al., 2019).

#### 1.4.3. Free radicals' detection

Free radicals were detected by electron paramagnetic resonance (EPR) (A300-10/12, Bruker Co., Ltd., German) and analyzed the signal peaks. The capture of  $\text{SO}_4^{\cdot-}$ ,  $\cdot\text{OH}$ , and  $\text{O}_2^{\cdot-}$  was 5,5-dimethyl-1-pyrroline-N-oxide (DMPO), and the capture of  $^1\text{O}_2$  was 2,2,6,6-tetramethyl-4-piperidone hydrochloride (TEMP).

Water (100 mL) was placed into the reactor with magnetic stirring, then adjusted the pH using 10 g/L and 1.0 g/L  $\text{NaOH}$  and kept the pH around 12. The PEC/PMS system was constructed with  $\text{TiO}_2$  as the counter electrode, CA as the working electrode and calomel electrode as the reference electrode, and then PMS was added to the solution. Under light irradiation condition, 30  $\mu\text{L}$  solution was measured at 0, 1, 5, and 10 min, respectively. DMPO was added to the solution to captured  $\text{SO}_4^{\cdot-}$  and  $\cdot\text{OH}$ . TEMP was added to another 30  $\mu\text{L}$  solution at 0, 1, 5, and 10 min to captured  $^1\text{O}_2$ . All mixtures were placed in the instrument to detected.

Based on the above operation, we changed the water to methanol to obtained the peaks of  $\text{O}_2^{\cdot-}$ , and DMPO was added to the 30  $\mu\text{L}$  of solution at 0, 1, 5, and 10 min to captured  $\text{O}_2^{\cdot-}$ ; TEMP was added to another 30  $\mu\text{L}$  of solution to captured  $^1\text{O}_2$ .

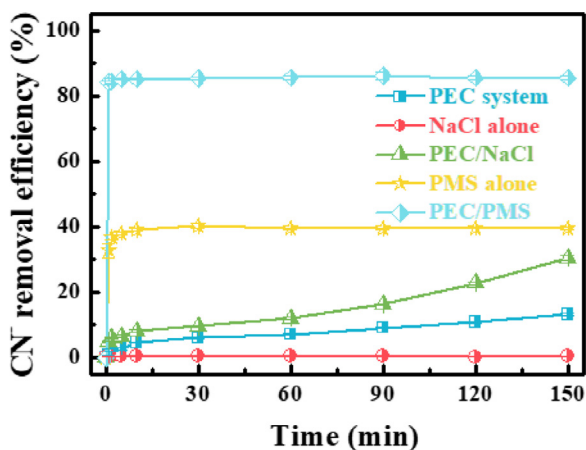
### 1.5. Characterization

The microstructure of catalyst was characterized by scanning electron microscopy (SEM, SU8010, HITACHI, Japan). The phase composition of catalyst was measured by X-ray diffraction (XRD, X'Pert 3 powder, Panalytical X'Pert Pro, Netherlands) with  $\text{Cu K}\alpha$  radiation ( $\lambda = 1.5418 \text{ \AA}$ ). X-ray photoelectron spectroscopy (XPS) measurements were recorded on a PHI-5300 Perkin-Elmer ESCA (USA) system operate at  $\text{Al K}\alpha$  source. *In-situ* Raman measurements were performed at room temperature using a Raman spectrometer (HR800, Horiba Scientific, France) with an excitation wavelength 514 nm. The electrochemical characterization including electrochemical impedance spectroscopy (EIS) measurements and photocurrent density test were taken on a CHI 660D electrochemical analyzer (Shanghai Chenhua Instruments Co., Ltd, Shanghai, China) using a standard three-electrode system.

## 2. Results and discussion

### 2.1. Characterization of $\text{TiO}_2$ NRs

The microstructure of fresh  $\text{TiO}_2$  NRs was analyzed using SEM and the results are showed in Fig. S1a. The SEM images revealed that  $\text{TiO}_2$  NRs covered the surface of the FTO glass and were tetragonal in shape with square top facets. Such a structure could engender many active sites for catalysis, which was a desirable condition for PEC applications (Cho et al., 2011). The phase structure of fresh  $\text{TiO}_2$  NRs was characterized by XRD (Fig. S1b). The phase structure was consistent with the rutile  $\text{TiO}_2$  phase, and the peaks located at  $2\theta$  of 36.1°, 41.2°, 62.7°, 69.0°, and 69.8° corresponded to the reflection planes (101), (111), (002), (301), and (112) of  $\text{TiO}_2$ , respectively. Fig. S2a displays the XPS survey spectra of  $\text{TiO}_2$ , and the peaks at approximately 284, 460, and 530 eV were attributable to C 1s, Ti 2p, and O 1s, respectively. The high-resolution O 1s spectrum has two peaks located at 529.9 and 531.6 eV (Fig. S2b), with the first peak corresponding to the binding Ti-O-Ti (Akhavan and Ghaderi, 2010). The second peak at 531.6 eV can be assigned to the -OH in -Ti(OH)-O-Ti-(OH)-, which was beneficial in forming the complex on the  $\text{TiO}_2$  surface (Hoffmann et al., 1995). Fig. S2c demonstrates the high resolution XPS spectrum of Ti 2p,

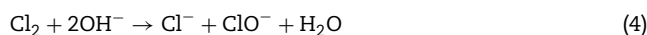


**Fig. 1** – Removal efficiency of  $\text{CN}^-$  in presence of NaCl alone, peroxymonosulfate (PMS) alone, photoelectrocatalysis (PEC) system, PEC/NaCl and PEC/PMS system. Reaction conditions:  $[\text{CN}^-] = 44.4 \text{ mg/L}$ , applied bias voltage =  $-1.2 \text{ V}$ ,  $\text{pH} = 12.0$  and light.

with the two peaks of Ti indicating the state of  $\text{Ti}^{4+}$  in the  $\text{TiO}_2$  NRs (Ye et al., 2017).

## 2.2. Effect of different additives on $\text{CN}^-$ removal efficiency

NaCl can be converted to active chlorine radicals during electrolysis which was used widely in industrial processing (Sasidharan Pillai and Gupta, 2016). To oxidative role of PMS and NaCl towards  $\text{CN}^-$  removal was studied comparatively. In addition,  $\text{CN}^-$  removal was investigated in different systems including PEC, PEC/NaCl, and PEC/PMS. As can be observed in Fig. 1, a slight removal of  $\text{CN}^-$  was apparent within 150 min when NaCl alone was added, while in the presence of PMS alone, the  $\text{CN}^-$  removal efficiency stood at 38.1% within 10 min. In a separate PEC system, the  $\text{CN}^-$  removal efficiency was only 17.0% within 150 min, and it was 30.0% in the PEC/NaCl system and 85.7% in the PEC/PMS system, respectively. The hypothesis drawn based on the above results was that with the mere addition of NaCl, the relative stability of NaCl failed to generate effective active radicals that were required to remove  $\text{CN}^-$ . While PMS alone was added, the  $\text{CN}^-$  removal efficiency increased to 38.1% since PMS could be catalyzed by  $\text{OH}^-$  to generate active species. As for the PEC system, the  $\text{CN}^-$  removal efficiency was only 17.0%, which could be attributed to the low activity of  $\bullet\text{OH}$  under alkaline conditions (Sun et al., 2018; Yang et al., 2013), although the photoanode  $\text{TiO}_2$  could produce a large amount of  $\bullet\text{OH}$  under light radiation. With the PEC/NaCl system, chloride ions ( $\text{Cl}^-$ ) were oxidized by  $\bullet\text{OH}$  to generate active chlorine, such as  $\text{Cl}\bullet$  and  $\text{ClO}\bullet$ . The conversion of chloride ions has been denoted in Eqs. (1)–(4). Active chlorine was favorable to the removal of  $\text{CN}^-$  (Tian et al., 2016). The reason for the PEC/PMS system obtaining a high  $\text{CN}^-$  removal efficiency of 85.7% was possibly because the PEC system could efficiently activate PMS to remove  $\text{CN}^-$ .



## 2.3. Effect of factors on PMS activation to remove $\text{CN}^-$

To analyze the effect of PEC on PMS activation, the effect of some parameters on  $\text{CN}^-$  removal was studied (Fig. 2). When the PMS concentrations increased from 0.10 mmol/L, 0.25 mmol/L, 0.50 mmol/L to 1.00 mmol/L, the  $\text{CN}^-$  removal efficiency rose from 26.4%, 38.1%, 66.0% to 95.9% (Fig. 2a). Compared to the system that used only PMS, the increase in  $\text{CN}^-$  removal efficiency was more obvious in the photocatalysis (PC)/PMS, electrocatalysis (EC)/PMS, and PEC/PMS systems, ascending from 26.4% for the PMS system to 51.1%, 58.2%, and 63.4% for the PC/PMS, EC/PMS, and PEC/PMS systems respectively, with a PMS concentration level of 0.10 mmol/L (Fig. 2b), and ascending from 38.1% for the PMS system to 69.1%, 79.1%, and 85.7% for the PC/PMS, EC/PMS, and PEC/PMS systems, respectively, when the PMS concentration was at 0.25 mmol/L (Fig. 2c). The  $\text{CN}^-$  were completely removed in PC/PMS, EC/PMS, PEC/PMS system when the PMS concentrations were 0.50 and 1.00 mmol/L (Fig. S3a and b). These results indicated that the  $\text{CN}^-$  removal efficiency increased with an increase in PMS concentration, and the presence of light and applied bias voltage could activate PMS to further improve  $\text{CN}^-$  removal efficiency. Thus, it was inferred that (1):  $\text{OH}^-$  could be oxidized by the hole ( $h^+$ ) generated via  $\text{TiO}_2$  with the presence of light to form  $\bullet\text{OH}$  to co-effect  $\text{CN}^-$  removal; (2):  $\text{TiO}_2$  would interact with PMS to generate active species in the presence of light. As established by previous studies (Qin et al., 2020; Sun et al., 2014), carbon materials could activate PMS to remove pollutants from wastewater. Therefore, in the EC/PMS system, a part of PMS would be activated by the CA cathode to generate active species for the removal of  $\text{CN}^-$ . Additionally,  $\text{CN}^-$  removal efficiency of the PEC/PMS system with differing applied bias voltage has been illustrated in Fig. 2d. When the applied bias voltage was  $-1.2 \text{ V}$ , the  $\text{CN}^-$  removal efficiency was 85.7%, while when the applied bias voltage was  $-0.5$  and  $-2.0 \text{ V}$ ,  $\text{CN}^-$  removal efficiency increased to 98.5% and 99.6%, respectively. The effect of the applied bias voltage on  $\text{CN}^-$  removal could be attributed to the activation of PMS by a photoanode and cathode. A small portion of the PMS would be adsorbed and activated by the cathode CA when the applied bias voltage was low. The impact that the cathode had on the activation of PMS diminished with an amplification in the applied bias voltage due to the PMS as well as anions moving to the photoanode when the applied bias voltage was high. The competitive adsorption of anions and PMS onto the  $\text{TiO}_2$  surface meant that  $\text{TiO}_2$  could only activate PMS partially, leading to it possessing the lowest  $\text{CN}^-$  removal efficiency. What was interesting to note was that when the applied bias voltage increased to  $-2.0 \text{ V}$ , the  $\text{CN}^-$  removal efficiency climbed to 99.6%, which could be ascribed to the effect engendered by the photoanode  $\text{TiO}_2$ .



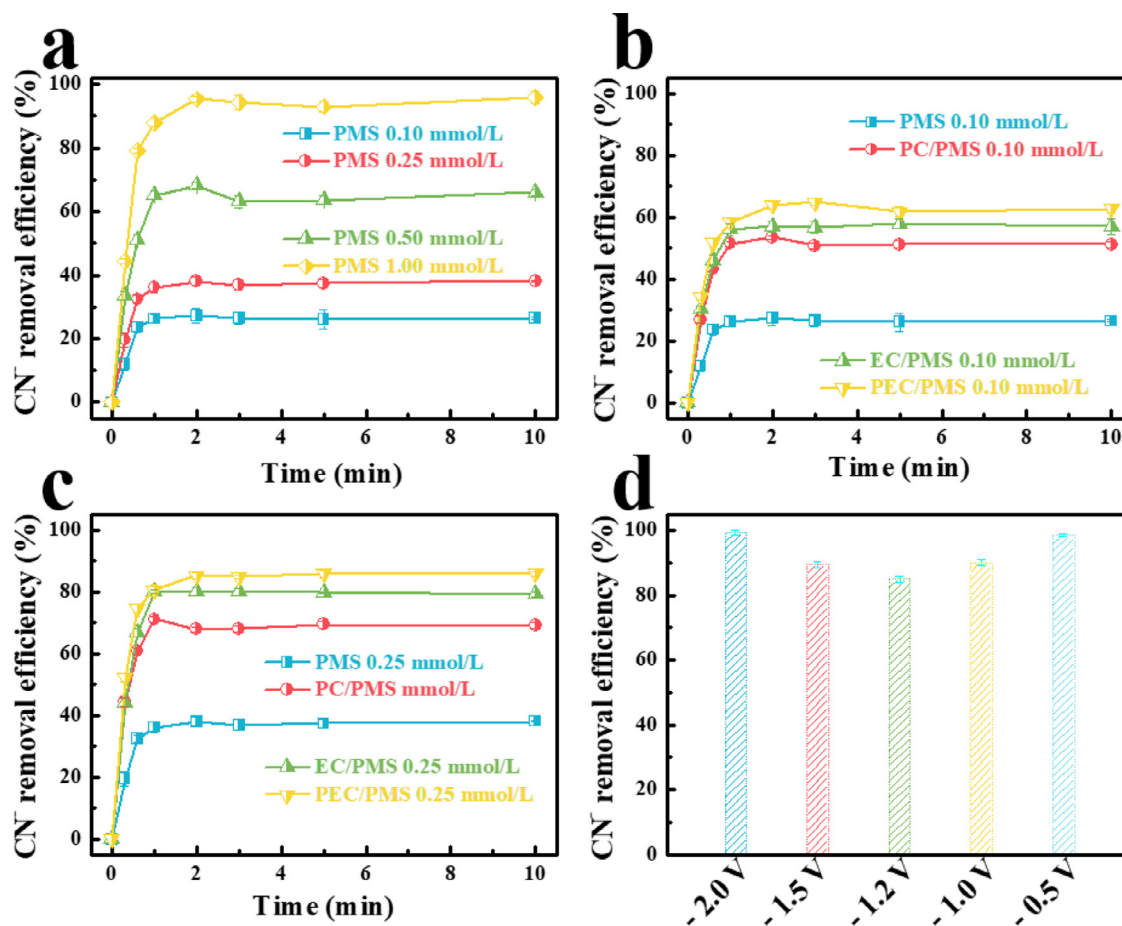


Fig. 2 – CN<sup>-</sup> removal efficiency at (a) different PMS concentration, (b) 0.10 mmol/L PMS with different system, (c) 0.25 mmol/L PMS with different system and (d) effect of different applied bias voltage on CN<sup>-</sup> removal. Reaction conditions: [CN<sup>-</sup>] = 44.4 mg/L, applied bias potential = -1.2 V, pH = 12.0 and light. PC: photocatalysis; EC: electrocatalysis.

#### 2.4. CN<sup>-</sup> removal mechanism

EPR free radical detection and a series of quenching experiments were performed to study the mechanism of CN<sup>-</sup> removal. The findings have been displayed in Fig. 3a and b. Unlike the traditional PMS activation mechanisms, SO<sub>4</sub><sup>-•</sup> and •OH were not detected in the PEC/PMS system. Moreover, although a strong signal of DMPO-O<sub>2</sub> was detected, the intensity of the signal decreased with the passage of time, indicating that O<sub>2</sub><sup>-•</sup> was the active species in the CN<sup>-</sup> removal process. Apart from O<sub>2</sub><sup>-•</sup>, an EPR test also detected the signal of 2,2,6,6-tetramethylpiperidinoxy (TEMPO), indicating that <sup>1</sup>O<sub>2</sub> was also active in CN<sup>-</sup> removal, with the perceived change in the intensity of the signal of <sup>1</sup>O<sub>2</sub> over time being similar to that of O<sub>2</sub><sup>-•</sup>. As is commonly known, it is possible to generate •OH from TiO<sub>2</sub> through h<sup>+</sup>, and this has been proved through the experiments discussed above; however, no indication of DMPO-OH was detected post the addition of PMS (not illustrated). The hypothesis for this outcome was that the PMS would react with TiO<sub>2</sub>, leading to the dissipation of •OH. Quenching experiments were carried out on the PEC/PMS system using an applied bias voltage of -0.5 V and a PMS concentration of 0.25 mmol/L. The potentially active

species during experimentation on CN<sup>-</sup> removal were primarily SO<sub>4</sub><sup>-•</sup>, •OH, <sup>1</sup>O<sub>2</sub>, O<sub>2</sub><sup>-•</sup>, and h<sup>+</sup>, and the scavengers were methanol, *tert*-butanol, *L*-histidine, *p*-benzoquinone, and ethylenediaminetetraacetic acid disodium salt (EDTA-2Na), respectively (Wang and Wang, 2020; Clifton and Huie, 1989). The scavengers and their corresponding rate constants have been recorded in Table 1. The results of the quenching experiments have been illustrated in Fig. 3c. After having added methanol to quench SO<sub>4</sub><sup>-•</sup> and *tert*-butanol to quench •OH, hardly any change was observed in the CN<sup>-</sup> removal efficiency, thus confirming that SO<sub>4</sub><sup>-•</sup> and •OH were not active species for CN<sup>-</sup> removal. When *L*-histidine was added to quench <sup>1</sup>O<sub>2</sub>, the CN<sup>-</sup> removal efficiency fell from 98.5% to 76.3%, indicating that <sup>1</sup>O<sub>2</sub> was one of the active species for CN<sup>-</sup> removal. A point to be noted is that the CN<sup>-</sup> removal rate decreased from 98.5% to 37.4% after the addition of *p*-benzoquinone to quench O<sub>2</sub><sup>-•</sup>, signifying that O<sub>2</sub><sup>-•</sup> was the primary active species for CN<sup>-</sup> removal. When EDTA-2Na was added to quench h<sup>+</sup>, the CN<sup>-</sup> removal efficiency diminished, indicating that h<sup>+</sup> was beneficial in CN<sup>-</sup> removal.

Recent study has proved that cyanate (CNO<sup>-</sup>) can be generated during the cyanide degradation as a byproduct (Guo et al., 2019). To further explore other compounds used in the CN<sup>-</sup>

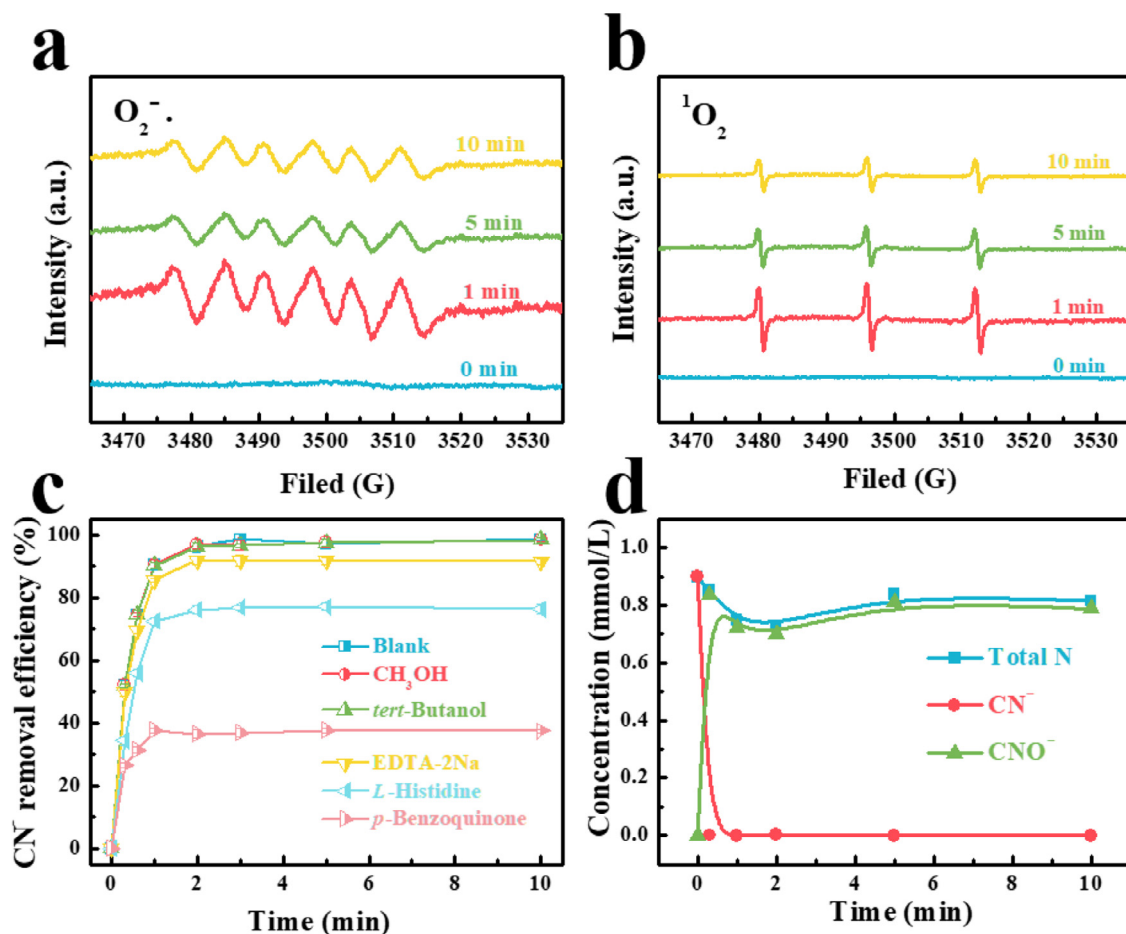


Fig. 3 – Electron paramagnetic resonance (EPR) spectra of (a)  $O_2^{\cdot-}$ , (b)  $^1O_2$ , (c) quenching experiments results and (d) production of  $CN^-$  removal analysis. Reaction conditions:  $[CN^-] = 44.4$  mg/L, applied bias voltage = - 0.5 V, pH = 12.0 and light. EDTA-2Na: ethylenediaminetetraacetic acid disodium salt.

Table 1 – Reactive species and their corresponding rate constant.

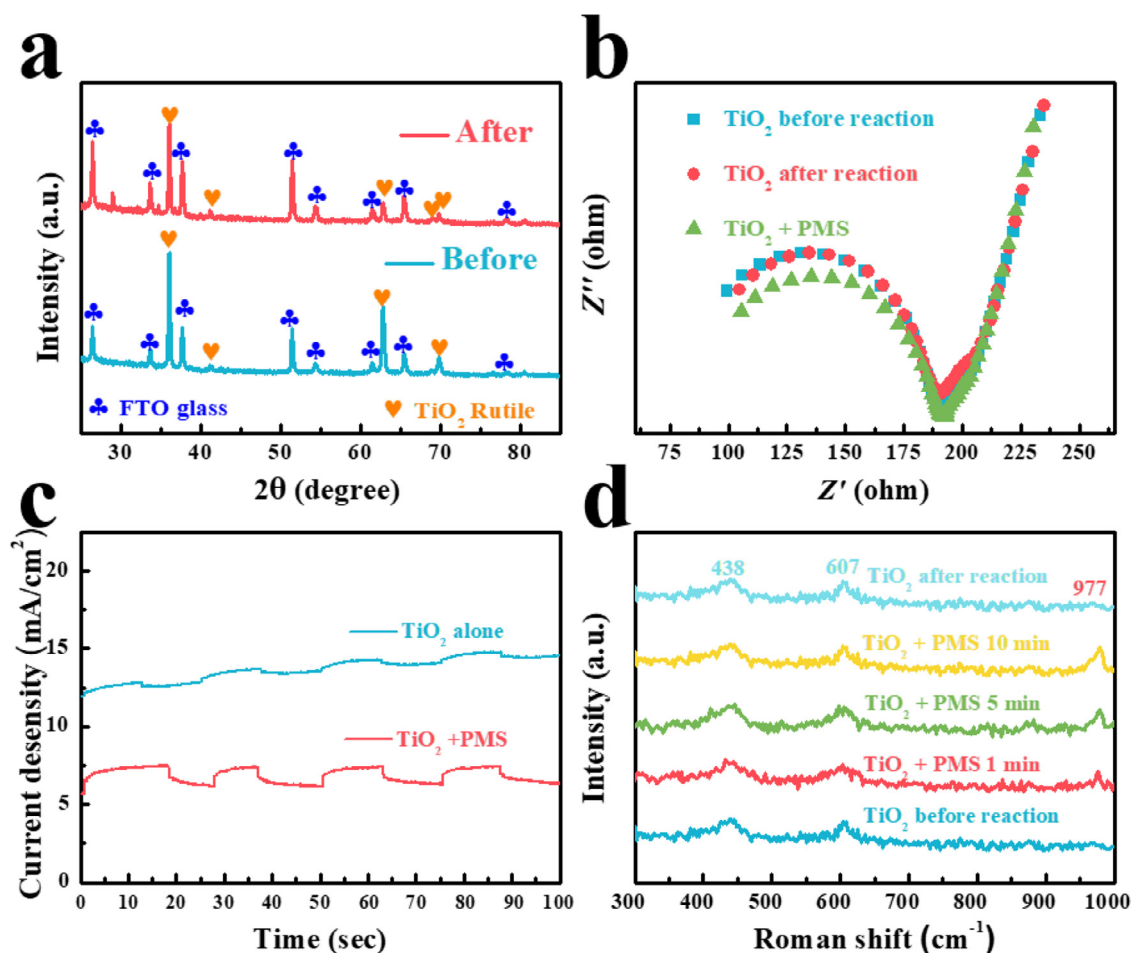
Reactive species	Scavenger	Rate constant	References
$SO_4^{\cdot-}$	Methanol	$\sim 10^7$	(Wang and Wang, 2020; Clifton and Huie, 1989)
$OH$	<i>tert</i> -Butanol	$\sim 10^8$	Clifton and Huie, 1989
$O_2^{\cdot-}$	<i>p</i> -Benzoquinone	$\sim 10^9$	Clifton and Huie, 1989
$^1O_2$	<i>L</i> -Histidine	$\sim 10^7$	Clifton and Huie, 1989
$h^+$	EDTA-2Na	$\sim na$	Clifton and Huie, 1989

na: no available;  $h^+$ : hole; EDTA-2Na: ethylenediaminetetraacetic acid disodium salt.

removal process, the elements of  $CN^-$ ,  $CNO^-$ , and total nitrogen (TN) were analyzed using UV-vis spectrophotometry and the results are illustrated in Fig. 3d. The initial 44.4 mg/L (0.90 mmol/L) concentration of  $CN^-$  was almost completely removed within 2 min, and the concentration of  $CNO^-$  rose from 0 to 0.84 mmol/L. The TN content exhibited a slight alteration, showing a downward trend during the initial 2 min, and then gradually rising to almost the original concentration levels. Since the sum of  $CN^-$  and  $CNO^-$  content was always equal to the amount of TN, it could be reliably stated that the element that was beneficial to the process of  $CN^-$  removal was

$CNO^-$ . Furthermore, the downward trend displayed by TN during the initial 2 min could have been caused by the adsorption of cathode CA.

It was deduced that the PEC system was beneficial to PMS activation for  $CN^-$  removal due to the higher removal efficiency displayed by the PEC/PMS system than that of PMS alone. For determining the impact of photoanode  $TiO_2$  and cathode CA on the activation of PMS, firstly, SEM images and XRD for used  $TiO_2$  were analyzed, with the findings being illustrated in Figs. S4 and 4a. No difference was observed in the SEM images and the XRD for fresh and used  $TiO_2$ , indicat-



**Fig. 4** – (a) X-ray diffraction (XRD) of fresh and used  $\text{TiO}_2$ , (b) electrochemical impedance spectroscopy (EIS) of  $\text{TiO}_2$  in presence of PMS and without, (c) photocurrent density of  $\text{TiO}_2$  in presence of PMS and without, and (d) in-situ Raman spectra of  $\text{TiO}_2$  in presence of PMS and without. Reaction conditions:  $[\text{PMS}] = 0.25 \text{ mmol/L}$ , applied bias voltage =  $-0.5 \text{ V}$ ,  $\text{pH} = 12.0$  and light. FTO: fluorine-doped tin oxide;  $Z'$ : real parts of the impedance;  $Z''$ : imaginary parts of the impedance.

ing the stability of the  $\text{TiO}_2$  NRs. Additionally, the EIS of fresh and used  $\text{TiO}_2$ , and the  $\text{TiO}_2$  from the PMS activation process were identified, and the same have been illustrated in Fig. 4b. The radius of the EIS curves of  $\text{TiO}_2$  in the presence of PMS is smaller than that of the curves for the fresh and used  $\text{TiO}_2$  NRs by themselves. This indicated that a minimal carrier transport resistance occurred after the PMS had been added. Fig. 4c displays the photocurrent density of  $\text{TiO}_2$  along with, as well as devoid of, PMS; the photocurrent density of  $\text{TiO}_2$  with PMS was higher than that of  $\text{TiO}_2$  devoid of PMS. Consequently,  $\text{TiO}_2$  and PMS could be combined to improve the separation efficiency of holes and photogenerated electrons, as well as the  $\text{CN}^-$  removal efficiency.

The in-situ Raman test was also used to study the interaction between  $\text{TiO}_2$  and PMS, and the findings for the same have been displayed in Fig. 4d. In the presence of only  $\text{TiO}_2$ , signal peaks appeared at  $438$  and  $606 \text{ cm}^{-1}$ , of which  $438 \text{ cm}^{-1}$  was a O-Ti-O torsional vibration, and  $606 \text{ cm}^{-1}$  was a O-Ti-O axial anti-symmetric stretching and equatorial bending vibration frequency. With the addition of PMS, peaks were detected

at  $438$ ,  $606$ , and  $977 \text{ cm}^{-1}$ , while the peak at  $977 \text{ cm}^{-1}$  dissipated without PMS. Thus, it could be inferred that the peak of  $977 \text{ cm}^{-1}$  was O-Ti-O-O-SO<sub>3</sub>.

To further investigate the impact that  $\text{TiO}_2$  had on PMS activation, the XPS spectrum for used  $\text{TiO}_2$  was analyzed (Fig. 5a-c). A new peak formed at nearly  $486 \text{ eV}$  and was assigned to the K element, which is derived from PMS (Fig. 5a). The peak at  $531.6 \text{ eV}$  was attributed to the -OH in -Ti(OH)-O-Ti-(OH)- and was enhanced, indicating that additional -Ti(OH)-O-Ti-(OH)- had formed after PMS activation (Fig. 5b). The transformation of O 1s at  $531.6 \text{ eV}$  could have been caused by the complex formed between  $\text{TiO}_2$  and PMS. In addition, a new peak at  $532.2 \text{ eV}$  was appeared, which could be attributed to the H<sub>2</sub>O molecule adsorption on the  $\text{TiO}_2$  surface (Hoffmann et al., 1995). The XPS spectrum of Ti remained unchanged (Fig. 5c), indicating the stability of  $\text{TiO}_2$ .

The influence that the CA cathode had on the activation of PMS was analyzed through a comparison of the  $\text{CN}^-$  removal efficiency of various CA and Pt cathodes as depicted in Fig. S5. The  $\text{CN}^-$  removal efficiency of the cathode Pt was approxi-

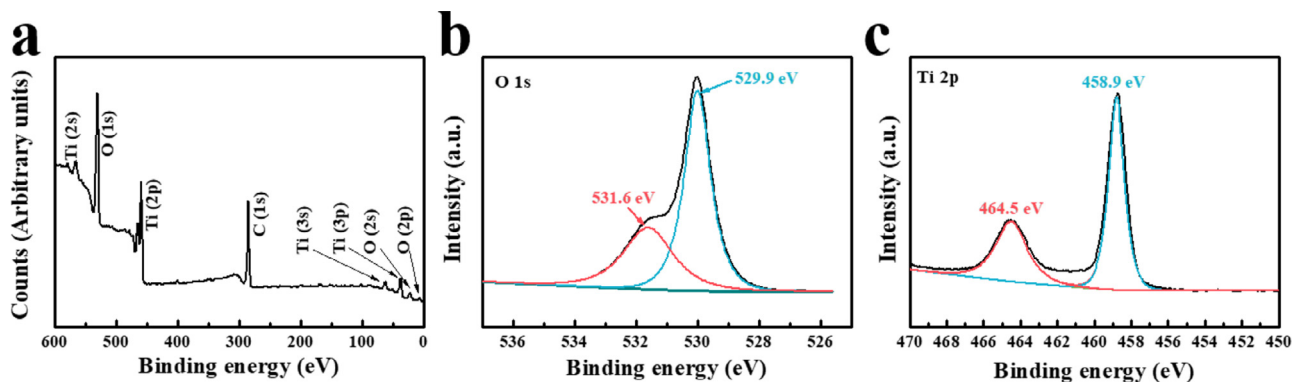


Fig. 5 – (a) X-ray photoelectron spectroscopy (XPS) survey spectrum of used TiO<sub>2</sub> and XPS spectra of (b) O 1s and (c) Ti 2p.

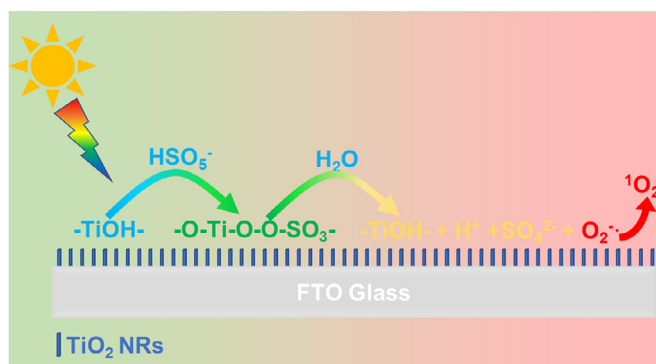
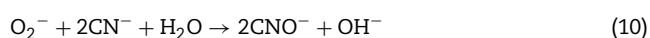
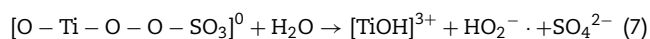
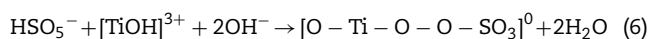


Fig. 6 – Mechanism of PMS activation by TiO<sub>2</sub> nanorods (NRs).

mately 83.4% and was lower than that of the cathode CA. Thus, it could be concluded that the cathode CA positively impacted PMS activation.

Based on the above experiments, a PMS activation mechanism employing TiO<sub>2</sub> was proposed, as in Fig. 6. The surface complex O-Ti-O-O-SO<sub>3</sub> would be formed between PMS and TiO<sub>2</sub> in the presence of light irradiation, which would then be transferred to -TiOH-, O<sub>2</sub><sup>-•</sup>, and SO<sub>4</sub><sup>2-</sup>. O<sub>2</sub><sup>-•</sup>, undergoing a series of changes to form <sup>1</sup>O<sub>2</sub>. The generation of O<sub>2</sub><sup>-•</sup> and <sup>1</sup>O<sub>2</sub> has been denoted in Eqs. (5)–(9) and the possible reactions that could occur in the CN<sup>-</sup> removal process have been denoted in Eqs. (10)–(11).



## 2.5. Kinetic analysis and stability test

In order to analyze the effect of PEC/PMS system on removal of CN<sup>-</sup>, the reaction kinetic constants (*k*) were calculated using the first-order and second-order dynamics model referred to the previous study (Feng et al., 2020). The removal rate equation can be described as the Eqs. (12) or (13). The curves of CN<sup>-</sup> concentration versus time with different initial PMS concentration were obtained and as Table S1 (first-order) and Table S2 (second-order). Then the *k* was calculated and the results as the Table 2.

First-order model:

$$\ln(c_t/c_0) = -k_1t \quad (12)$$

Second-order model:

$$1/c_t - 1/c_0 = k_2t \quad (13)$$

where *c<sub>t</sub>* and *c<sub>0</sub>* are the concentration at time *t* and the initial concentration, respectively.

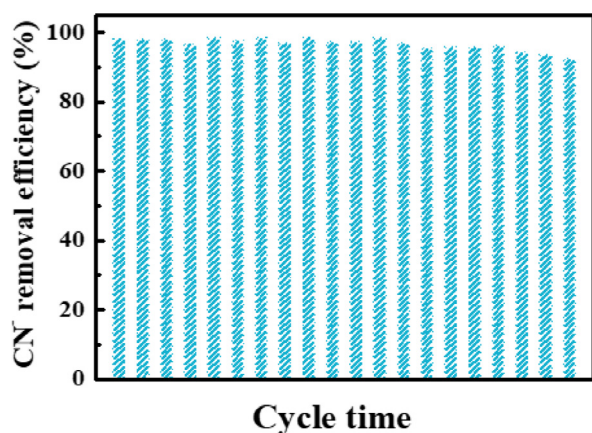
The R<sup>2</sup> for the first-order model is consistently higher than that of the second-order model, it was demonstrated that the removal kinetics of CN<sup>-</sup> follows the first-order model. The *k* of PEC/PMS system was increasing with the PMS concentration increased, the reason for that mainly resulting from the more PMS was activated by TiO<sub>2</sub> to forms O<sub>2</sub><sup>-•</sup> and <sup>1</sup>O<sub>2</sub>. These active species can quickly oxidize the CN<sup>-</sup> and achieve the purpose of removing CN<sup>-</sup>. Therefore, the PEC/PMS system can be considered as an effective technology to remove cyanide.



**Table 2 – Reaction kinetic constants ( $k$ ) in different peroxymonosulfate (PMS) concentration in photoelectrocatalysis (PEC) system.**

System	PMS concentration (mmol/L)	$k_1$	$R^2$	$k_2$	$R^2$
PEC/PMS	0.10	0.4569	0.8767	0.8375	0.8575
	0.25	0.8671	0.9094	2.8517	0.8914
	0.50	2.2558	0.9882	14.242	0.8440
	1.00	2.6665	0.9894	22.403	0.8902

$k_1$ :  $k$  of first-order model;  $k_2$ :  $k$  of second-order model.

**Fig. 7 – Stability analysis of PEC system.**

The stability of the catalyst is one of the important indicators in measuring excellence in a pollutant removal system. In this study, the PEC/PMS system was cyclically tested 20 times, with the findings being illustrated in Fig. 7. In this system, the primary function of the  $\text{TiO}_2$  photoanode was to activate the PMS by forming a complex on the surface of the  $\text{TiO}_2$ . The complex was unstable and decomposed into active species, which failed to alter the structure of  $\text{TiO}_2$ .

### 3. Conclusions

The PEC system constructed with  $\text{TiO}_2$  as the photoelectric anode and CA as the cathode activates the PMS to remove  $\text{CN}^-$  from wastewater, attaining a removal efficiency as high as 98.5% with light irradiation, an applied bias voltage of -0.5 V, and a PMS concentration of 0.25 mmol/L. The methodology for  $\text{CN}^-$  removal was analyzed via EPR and quenching experiments, and  $\text{O}_2^{\cdot-}$  and  $^1\text{O}_2$  were found to be the dominant active species rather than  $\text{SO}_4^{\cdot-}$  and  $\cdot\text{OH}$ . It was also successfully established that PMS was activated by  $\text{TiO}_2$  through a comparison using the Raman test, XRD, EIS, and XPS for fresh and used  $\text{TiO}_2$ . Moreover, this system offers additional advantages such as low cost, technological simplicity, stability of performance, reusability, and broad-spectrum application prospects in the field of water body restoration.

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### Appendix A Supplementary data

Supplementary material associated with this article can be found in the online version at [doi:10.1016/j.jes.2021.08.054](https://doi.org/10.1016/j.jes.2021.08.054).

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